

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

1. (Currently Amended): A method of for manufacture of a granulate containing at least one polyvinylacetal, said method comprising converting characterized in that a polyvinylacetal-containing polyvinylacetal-containing composition is converted into a the molten state by heating to 100 to 340 °C in a single or double screw extruder, and granulating the resultant material granulated corresponding to the desired particle sizes.

2. (Cancelled):

3. (Cancelled):

4. (Currently Amended): The method in accordance with Claim 1, wherein characterized in that the granulating of the resultant material is performed by hot pelletization granulate is manufactured by hot cutting down, cold cutting down or strand extrusion.

5. (Currently Amended): The method in accordance with Claim 1, wherein characterized in that during conversion to the molten state a foaming agent is added to the polyvinylacetal-containing composition.

6. (Currently Amended): The method in accordance with Claim 1, wherein characterized in that at least one part of the polyvinylacetal-containing composition is introduced into said screw extruder transferred via at least one side stream inlet into an extruder.

7. (Currently Amended): The method in accordance with claim 6, wherein characterized in that at least 90 wt% of the polyvinylacetal-containing composition is introduced into said screw extruder transferred via at least one side stream inlet into the extruder.

8. (Currently Amended): The method in accordance with claim 6, ~~characterized in that the~~ said at least one side stream inlet is cooled by means of which at least one part of the polyvinylacetal-containing composition is fed into the extruder.

9. (Currently Amended): The method in accordance with Claim 1, characterized in that the region of the extruder from the main inlet up to a length equal to or at least  $15 \cdot L/D$  times the diameter of the screw is cooled, wherein L represents the length of the screw and D represents the diameter of the screw.

10. (Currently Amended): The method in accordance with Claim 1, ~~characterized in that~~ wherein at least one of the extruder screws is cooled.

11. (Currently Amended): The method in accordance with claim 10, characterized in that the screw is cooled over the range of the extruder from the main inlet up to a length equal to or at least  $10 \cdot L/D$ , wherein L represents the length of the screw and D represents the diameter of the screw.

12. (Currently Amended): The method in accordance with Claim 8, ~~characterized in that~~ the temperature of the cooling means used to cool said at least one side stream inlet is less than or equal to the glass transition temperature of the polyvinylacetal-containing composition, which contains at least one polyvinylacetal.

13. (Currently Amended): The method in accordance with Claim 1, wherein ~~characterized in that~~ the temperature in feeding of the polyvinylacetal-containing composition into the molten state is changed.

14. (Currently Amended): The method in accordance with claim 9, ~~characterized in that the temperature~~ wherein, during the conversion of the polyvinylacetal-containing composition into the molten state, the temperature in said screw extruder is increased.

15. (Currently Amended): The method in accordance with Claim 1, wherein ~~characterized in that~~ gaseous compounds, which arise upon conversion of the polyvinylacetal-containing composition into the molten state, are removed from the composition.

16. (Currently Amended): The method in accordance with claim 15, wherein ~~characterized in that~~ a part of the gaseous compounds is removed via the main entry port of the screw extruder.

17. (Currently Amended): The method in accordance with Claim 6, wherein ~~characterized in that~~ the side stream input of said at least one part of the polyvinylacetal-containing composition takes place by means of a dosing device with one or two screw-conveyors.

18. (Currently Amended): The method in accordance with Claim 6, wherein ~~characterized in that~~ the diameter of the extruder screw or screws ~~diameter~~ is larger than the ~~screw~~ diameter of the one or two screw-conveyors of the ~~side stream~~ dosing device.

19. (Currently Amended): The method in accordance with Claim ~~6~~ 18, wherein ~~characterized in that~~ the ratio of the screw diameter of the extruder to the screw diameter of the side stream dosing device lies in the range from 1.1:1 to 10:1.

20. (Currently Amended): The method in accordance with Claim 6, wherein ~~characterized in that~~ the temperature in the region of the side stream dosing device is less than or equal to the glass transition temperature of the polyvinylacetal-containing composition ~~which contains at least one polyvinylacetal~~.

21. (Currently Amended): The method in accordance with Claim 1, wherein ~~characterized in that~~ the polyvinylacetal-containing composition ~~for manufacture of granulate which contains the polyvinylacetal~~, has a glass transition temperature greater than or equal to 0 °C.

22. (Currently Amended): The method in accordance with Claim 1, wherein  
~~characterized in that the polyvinylacetal-containing composition for manufacture of granulate~~  
~~which contains the polyvinylacetal, comprises 95 wt% polyvinylacetal polyvinylectal.~~

23. (Currently Amended): The method in accordance with Claim 1, wherein  
~~characterized in that the polyvinylacetal-containing composition for manufacture of granulate,~~  
~~which contains the polyvinylacetal, contains at the most 2 wt% external softener.~~

24. (Previously Presented) The granulate obtainable according to a method in  
accordance with Claim 1.

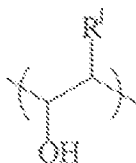
25. (Withdrawn: Currently Amended): A method according to claim 1, wherein  
the resultant ~~The granulate produced according to claim 24, characterized in that it has a bulk~~  
~~density, in accordance with~~ with Standard 543, of greater than 350 g/l.

26. (Withdrawn: Currently Amended): A method according to claim 1, wherein  
the resultant ~~The granulate in accordance with claim 24, characterized in that it has a  $d_{50}/d_{90}$~~   
 ~~$D_{50}/D_{90}$  value greater than 0.70.~~

27. (Withdrawn: Currently Amended): A method according to claim 1, wherein  
the resultant ~~The granulate in accordance with claim 24, characterized in that in relation to the~~  
~~total weight it contains at least 50.0 wt% of at least one polyvinylacetal, with respect to the~~  
total weight.

28. (Withdrawn: Currently Amended): A method according to claim 27, wherein  
in the resultant ~~The granulate in accordance with claim 27, characterized in that the~~  
polyvinylacetal is obtainable through reaction of at least a polymer (A) with at least a  
compound (B), wherein the polymer (A) contains

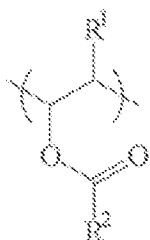
1.0 to 100.0 wt% structural units of formula (1)



(1)

wherein R¹ ~~is~~ denotes hydrogen or methyl,

b.) 0 to 99.0 wt% structural units of formula (2)



(2)

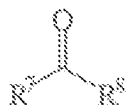
wherein R² ~~is~~ represents hydrogen or an alkyl group with 1 to 6 carbon atoms,

c.) 0 to 70.0 wt% structural units of formula (3)



(3)

wherein ~~Wherein~~ R³, R⁴, R⁵ and R⁶, are, ~~denote~~ in each case independently of each other, groups with a molecular weight in the range from 1 to 500 g/mol, and wherein the compound (B) satisfies formula (4),



(4)

wherein ~~Wherein~~ R⁷ and R⁸, in each case independently of each other, are hydrogen, COOH, COOM, an alkyl group with 6 to 12 carbon atoms, or an aryl

group 6 to 12 carbon atoms, and wherein M is a metal cation or if applicable an alkylated ammonium cation.

29. (Withdrawn: Currently Amended): A method according to claim 1, wherein the resultant ~~The granulate in accordance with Claim 24, characterized in that it contains other additives.~~

30. (Withdrawn: Currently Amended): A method according to claim 1, wherein the resultant ~~The granulate in accordance with Claim 24, characterized in that it furthermore contains fiber-strengthening materials.~~

31. (Withdrawn: Currently Amended): A method according to claim 30, wherein the resultant ~~The granulate in accordance with claim 30, characterized in that it contains short glass fibers, long glass fibers, aramid fibers and/or carbon fibers as fiber strengthening material.~~

32. (Withdrawn): The granulate in accordance with Claim 24, characterized in that one solution prepared from the obtained granulate has a yellow value less than or equal to 3.

33. (Withdrawn: Currently Amended): A method according to claim 28, wherein ~~The granulate in accordance with Claim 24, characterized in that the polyvinylacetal~~ polyvinylacetal has a glass transition temperature greater than or equal to 0 °C.

34. (Withdrawn; Currently Amended): In a method of preparing a polyvinylacetal solution, the improvement wherein said polyvinylacetal solution is prepared from granulates produced according to the method of claim 1 ~~The use of a granulate according to Claim 24 for preparation of a polyvinylacetal solution.~~

35. (Withdrawn; Currently Amended): In a method of preparing a film, the improvement wherein said film is prepared from granulates produced according to the

method of claim 1 ~~The use of a granulate according to Claim 24 for preparation of a film.~~

36. (Withdrawn; Currently Amended): In a method of preparing laminated safety glasses using a polyvinylacetal film, the improvement wherein said film is prepared from granulates produced according to the method of claim 1 ~~The use of a granulate according to Claim 24 for the manufacture of laminated safety glasses.~~

37. (Withdrawn): The use of a granulate according to Claim 24 as binding agent.

38. (New): The method in accordance with Claim 1, wherein granulating of the resultant material is performed by cold pelletization.

39. (New): The method in accordance with Claim 1, wherein said polyvinylacetal-containing composition is converted into the molten state by heating to 130 to 200 °C in said single or double screw extruder.

40. (New): The method in accordance with Claim 1, wherein the resultant granules have a  $d_{10}/d_{100}$  value that is greater than 0.2, a  $d_{50}/d_{100}$  value that is greater than 0.2, and a  $d_{50}/d_{90}$  value that is greater than 0.70.

41. (New): The method in accordance with Claim 1, wherein the resultant granules have a  $d_{10}/d_{100}$  value that is greater than 0.99, a  $d_{50}/d_{100}$  value that is greater than 0.99, and a  $d_{50}/d_{90}$  value that is greater than 0.99.

42. (New): A method according to claim 1, wherein the resultant granulate has a bulk density, in accordance with Standard 543, of greater than 550 g/l.

43. (New): A method according to claim 1, wherein the resultant granulate has a bulk density, in accordance with Standard 543, of greater than 600 g/l.

44. (New): A method according to claim 1, wherein the resultant granulate has a

bulk density, in accordance with Standard 543, of greater than 650 g/l.

45. (New): A method according to claim 1, wherein the resultant granulate has a bulk density, in accordance with Standard 543, of greater than 700 g/l.